

Robust Data Reconciliation to Determine Basic Oxygen Furnace Set-points

IFAC MMM 2009

Workshop on Automation in Mining, Mineral and Metal Industry

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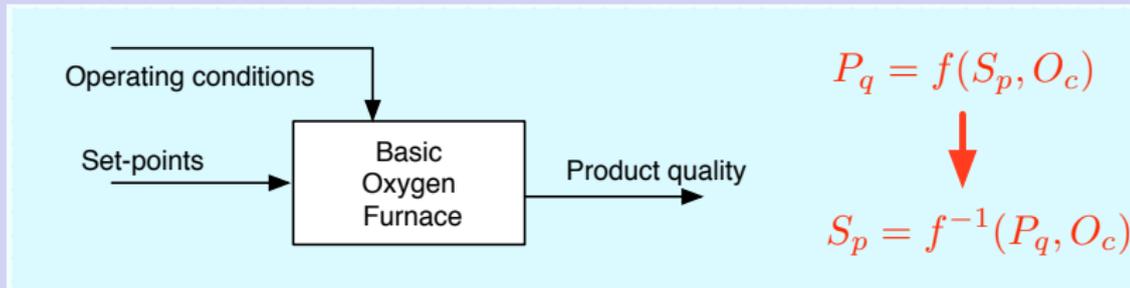


- 1 Motivations and process description
- 2 Data reconciliation
- 3 Application
- 4 Improvement
- 5 Conclusion

1. Batch process set-points determination

Industrial problem

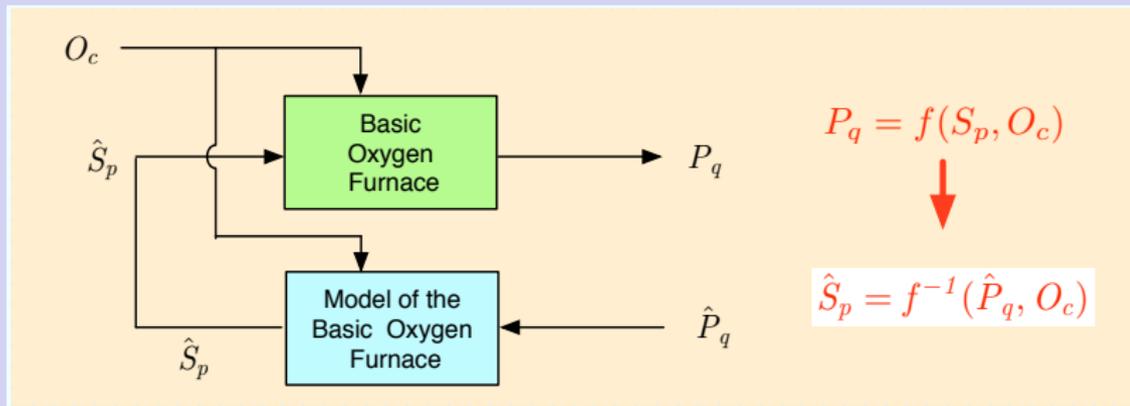
- Determination of the control system set-points of batch processes in order to reach given product specifications thanks to a process model.
- Process models are inaccurate.
- Measurements are corrupted by different errors (noises, biases) or are lacking



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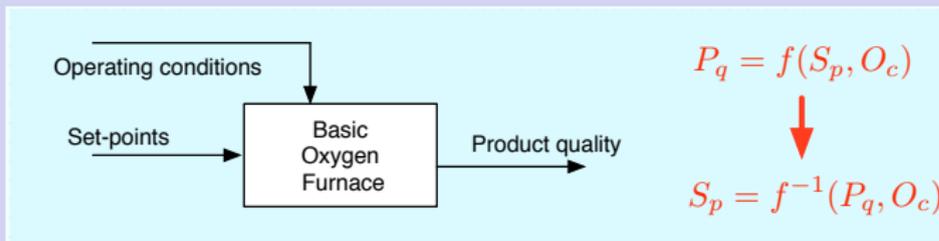
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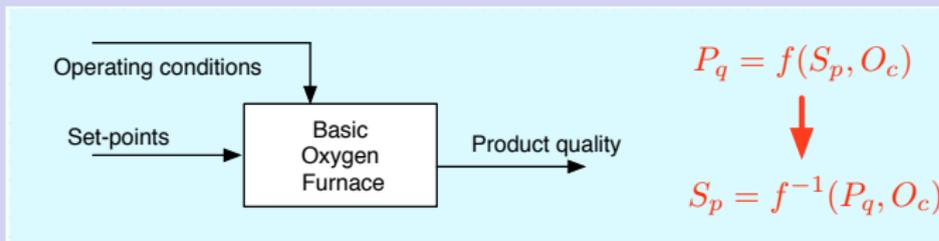
Objectives and proposed method

- Necessity to have consistent measurements → use of data reconciliation method
- Ensure the monitoring of system component deterioration along the time (due to wear-out, clogging) → model parameter estimation

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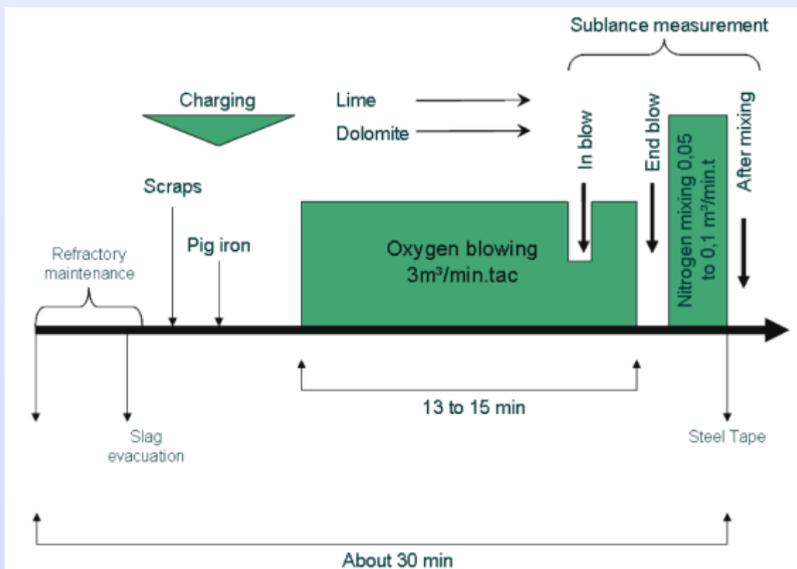
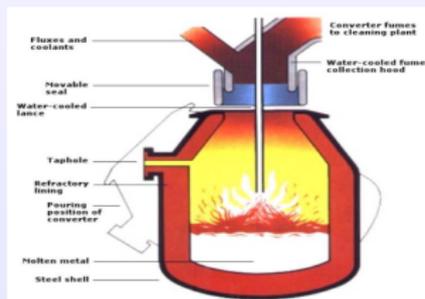


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⇒ Use of method allowing **simultaneously** data reconciliation

1. Operation scheduling of a Basic Oxygen Furnace



1. Application target - the Basic Oxygen Furnace (BOF)

Main objectives of a BOF

- To refine the hot metal produced in a blast furnace into raw liquid steel
- To decarburize and remove phosphorus from the hot metal
- To optimize the steel temperature so that any further treatments prior to casting can be performed with minimal reheating or cooling of the steel

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Setup problem and means

- To determine the quantity of **iron ore to add** and the **oxygen volume to blow** to reaching the target of Carbon rate in steel and the temperature defined for each heat (batch) by the given product specification
- Static load computation based on a model formed by comprehensive **heat and mass balances**

“Classical” data reconciliation

- Model of the system : a set of measurements x_i and a set of constraints f

$$\begin{cases} x_i = x_i^* + \varepsilon_{x_i} \\ f(x_i^*, a) = 0 \end{cases}, \quad i = 1, \dots, N,$$

where x_i^* are the state variables and a the **known** model parameters.

- Hypothesis

$$\mathcal{H}_1 : \varepsilon_{x_i} \sim \mathcal{N}(0, V)$$

or

$$\mathcal{H}_2 : \varepsilon_{x_i} \in [-\delta \quad +\delta]$$

- Data reconciliation: estimate the state variables of the system. For example, with \mathcal{H}_1 :

$$\begin{aligned} \hat{x}_i &= \arg \min_{x_i^*} \Phi = \|x_i - x_i^*\|_{V^{-1}}^2 \\ \text{s.t.} \quad & f(x_i^*, a) = 0 \end{aligned}$$

2. Theoretical formulation: data reconciliation with uncertain model

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Interests

- Provide coherent data (more likelihood data than raw measurements)
- Allow to detect and isolate sensor faults
- Estimate unmeasured state variables

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Constraint: the model is assumed to be perfectly known

2. Historical point of view

- Importance of covariance in mass balancing of particle size distribution data
 - Design and upgrade of process plant instrumentation
 - Data reconciliation and gross error detection
 - Fault detection and diagnosis in industrial systems
 - Redescending estimators for data reconciliation and parameter estimation
 - Robust data reconciliation based on a generalized objective function
 - Data reconciliation in gas pipeline systems
 - Data reconciliation: a robust approach using contaminated distribution. Application in mineral processing for multicomponent products
 - Mass balance equilibration: a bilinear case with a robust approach using contaminated distribution
 - Using sub-models for dynamic data reconciliation.
 - In-Line monitoring of bulk polypropylene reactors based on data reconciliation procedures
 - Adaptation and testing of data reconciliation software for CAPE-OPEN compliance
- | | |
|--|------|
| C. Bazin, D. Hodouin | 1999 |
| J. Romagnoli | 2000 |
| S. Narasimhan, C. Jordache | 2000 |
| L.H. Chiang, E.L. Russell, R.D. Braatz | 2001 |
| N. Arora, L.T. Biegler | 2001 |
| D. Wang, J.A. Romagnoli | 2002 |
| M.J. Bagajewicz, E. Cabrera | 2003 |
| M. Alhaj-Dibo, D. Maquin, J. Ragot | 2004 |
| J. Ragot, M. Chadli, D. Maquin | 2005 |
| L. Lachance, A. Desbiens, D. Hodouin | 2006 |
| D. Martinez Prata, E.L. Lima, J.C. Pinto | 2008 |
| E. Radermecker, M.N. Dumont, G. Heyen | 2009 |

2. Theoretical formulation: data reconciliation with uncertain model

Proposed approach – Simultaneous data reconciliation and parameter estimation

- The considered system is modeled using a set of measurements x_i , a set of constraints f and an *a priori* knowledge of the parameter values.

$$\begin{cases} x_i = x_i^* + \varepsilon_{x_i} \\ f(x_i^*, a^*) = 0 \end{cases}, \quad i = 1, \dots, N$$

- Uncertainties on the knowledge of the parameters are expressed with a "pseudo-measurement" equation:

$$a = a^* + \varepsilon_a, \quad \varepsilon_a \sim \mathcal{N}(0, W)$$

- Simultaneous estimation problem (maximum likelihood approach)

$$p_{x_i} = \frac{1}{(2\pi)^{\nu/2} |V|^{1/2}} \exp\left(-\frac{1}{2}(x_i^* - x_i)^T V^{-1}(x_i^* - x_i)\right)$$

$$p_a = \frac{1}{(2\pi)^{\rho/2} |W|^{1/2}} \exp\left(-\frac{1}{2}(a^* - a)^T W^{-1}(a^* - a)\right)$$

$$\begin{aligned} (\hat{x}_i, \hat{a}) &= \arg \min_{(x_i, a)} \mathcal{V} = \prod_{i=1}^N p_{x_i} p_a \\ \text{s.t.} \quad & f(x_i^*, a^*) = 0 \end{aligned}$$

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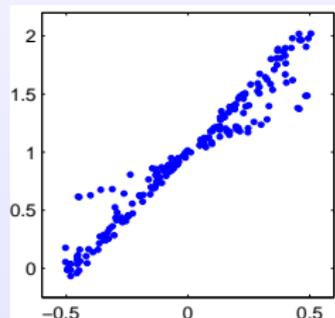
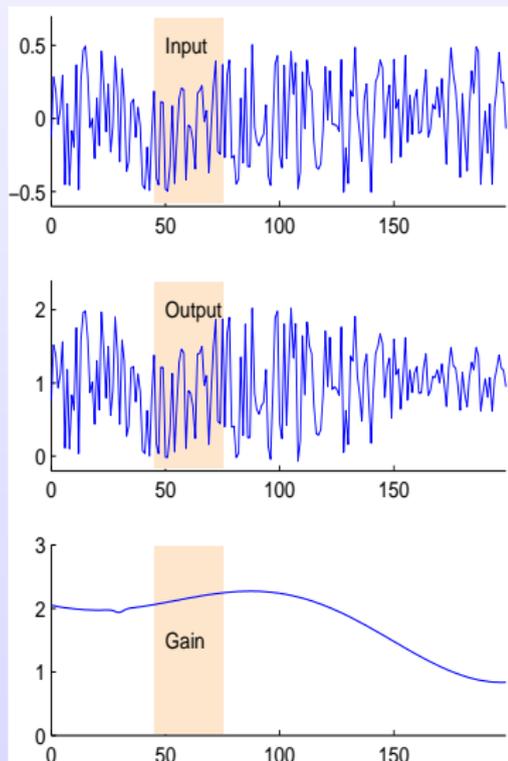
2. Theoretical formulation: data reconciliation with uncertain model

Some difficulties and extensions

- Unmeasured variables
- Dynamic model
- Convergence proof

2. An academic example: basic formulation of data reconciliation

Data



Model

$$y^* - ax^* = 0$$

Measurement

$$x_i = x_i^* + \varepsilon_{x_i}$$

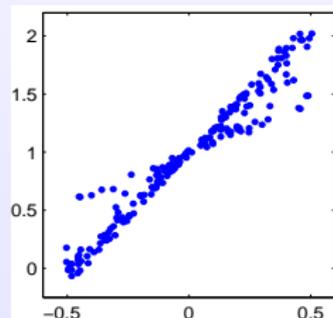
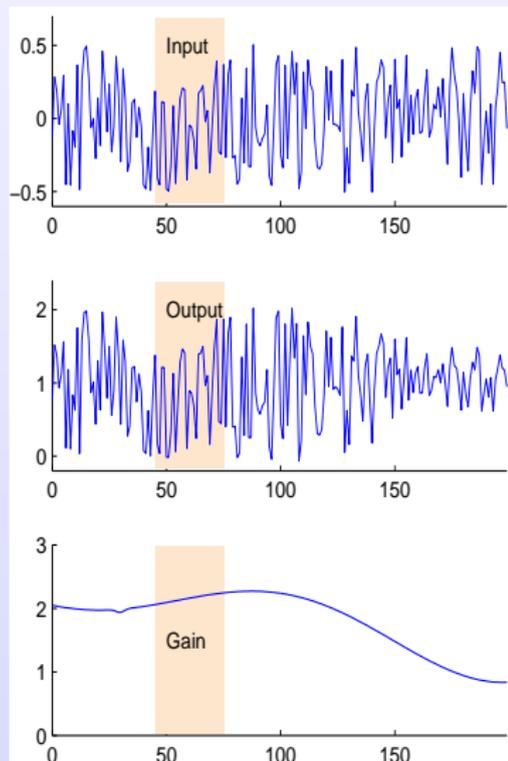
$$y_i = y_i^* + \varepsilon_{y_i}$$

Lagrange function

$$\mathcal{L} = \sum_{i=k}^{k+N} \left(\frac{x_i - x_i^*}{\sigma_{x,i}} \right)^2 + \left(\frac{y_i - y_i^*}{\sigma_{y,i}} \right)^2 + \lambda_i (y_i^* - ax_i^*)$$

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$$y^* - ax^* = 0$$

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2. An academic example: proposed formulation of data reconciliation

Optimality equation

$$\mathcal{L} = \sum_{i=k}^{k+N} \left(\frac{x_i - x_i^*}{\sigma_{x,i}} \right)^2 + \left(\frac{y_i - y_i^*}{\sigma_{y,i}} \right)^2$$
$$+ \lambda_i (y_i^* - \mathbf{a}x_i^*)$$
$$\begin{cases} \mathbf{V}_x^{-1}(\hat{\mathbf{x}} - \mathbf{x}) - \lambda \mathbf{a} = 0 \\ \mathbf{V}_y^{-1}(\hat{\mathbf{y}} - \mathbf{y}) + \lambda = 0 \\ \hat{\mathbf{y}} - \mathbf{a}\hat{\mathbf{x}} = 0 \\ \lambda^T \hat{\mathbf{x}} = 0 \end{cases}$$

Numerical solution may be obtained

2. An academic example: proposed formulation of data reconciliation

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Numerical solution may be obtained

Implementation

Perform estimation on a time window of length N :

$$W_1 = [1 \quad N]$$

Then, perform estimation on a time window of length N

$$W_2 = [2 \quad N + 1]$$

...

2. An academic example: proposed formulation of data reconciliation

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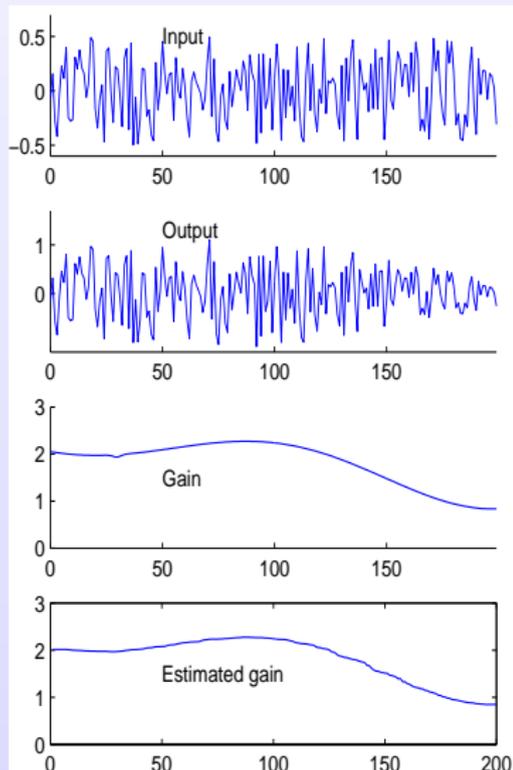
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2. Theoretical formulation: data reconciliation with uncertain model

Practical implementation

$$\begin{array}{c} 1 \\ \text{---} \\ \text{①} \end{array} \begin{array}{c} N \\ \text{---} \end{array} X_1, \dots, X_N, a^{(0)} \longrightarrow \hat{X}_1, \dots, \hat{X}_N, \hat{a}^{(1)}$$

$$\begin{array}{c} 2 \\ \text{---} \\ \text{②} \end{array} \begin{array}{c} N+1 \\ \text{---} \end{array} X_2, \dots, X_{N+1}, a^{(1)} \longrightarrow \hat{X}_2, \dots, \hat{X}_{N+1}, \hat{a}^{(2)}$$

$$\begin{array}{c} 3 \\ \text{---} \\ \text{③} \end{array} \begin{array}{c} N+2 \\ \text{---} \end{array} X_3, \dots, X_{N+2}, a^{(2)} \longrightarrow \hat{X}_3, \dots, \hat{X}_{N+2}, \hat{a}^{(3)}$$

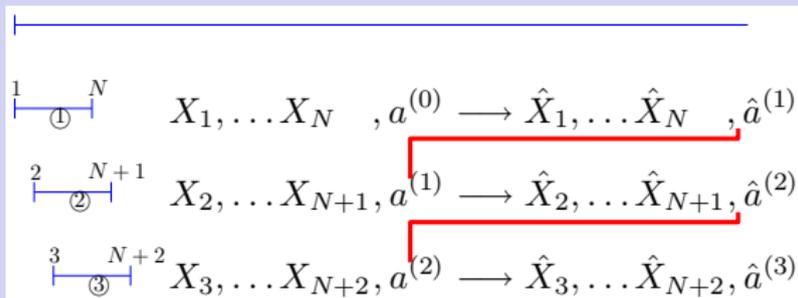
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Interests of simultaneous data reconciliation and parameter estimation

- Provide coherent data (state variables + model parameter)
- Allow the monitoring of model parameter (drifts, component deterioration)
- Feed model adaptation algorithms for the next batch

3. Application to a simplified BOF process

Mass and heat balances

$$\begin{aligned}(-0.99 + x_3^*)x_2^* + (0.95 - x_6^*)x_5^* + a_1^* &= 0 \\0.001x_1^* - (0.007 + 3x_3^*)x_2^* - (0.024 + a_2^*x_6^*)x_5^* + 1.19 &= 0 \\(-4e-3x_3^*x_4^* + a_3^*x_3^* - 2e-6x_4^* + 3e-3)x_2^* \\-(1e-4x_6^*x_7^* + 0.12x_6^* + 2e-6x_7^* + 2e-3)x_5^* - 0.256 &= 0\end{aligned}$$

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Data

Table: Measurement ranges and accuracies

Variable	x_1	x_2	x_3	x_4	x_5	x_6	x_7
Min value	63593	3.76	4.7	4000	3.71	7.27	1.04
Max value	96750	4.79	5.74	5232	4.68	12.96	2,02
Standard deviation	3339	0.19	0.24	202	0.19	0.48	0.052

Table: "A priori" parameter knowledge

Parameter	a_1	a_2	a_3
Nominal value	17.85	0.4	16
Standard deviation	0.893	0.02	0.8

3. Application to a simplified BOF process

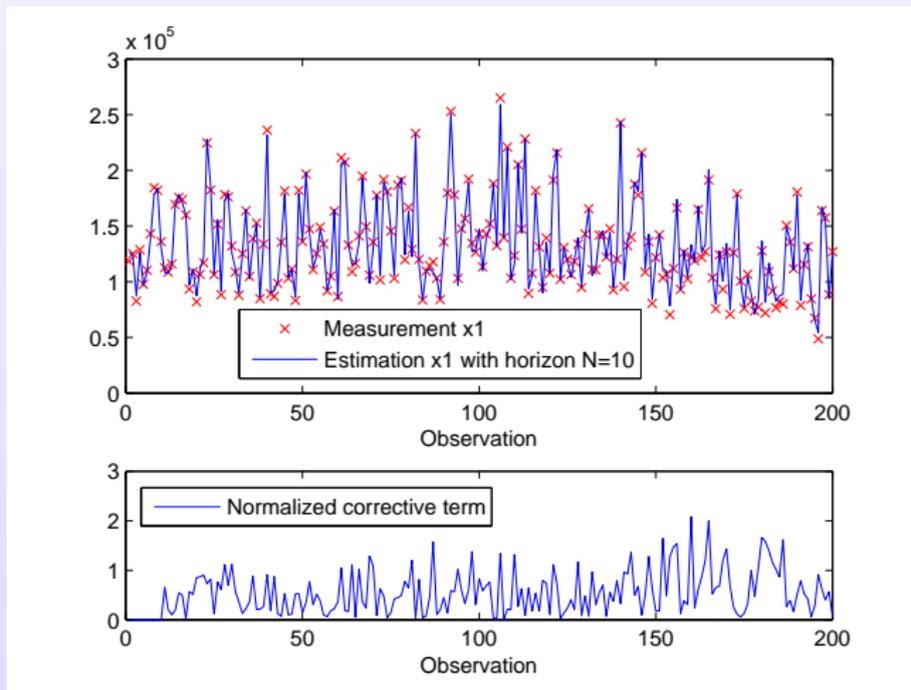


Figure: x_1 state estimation and measurement

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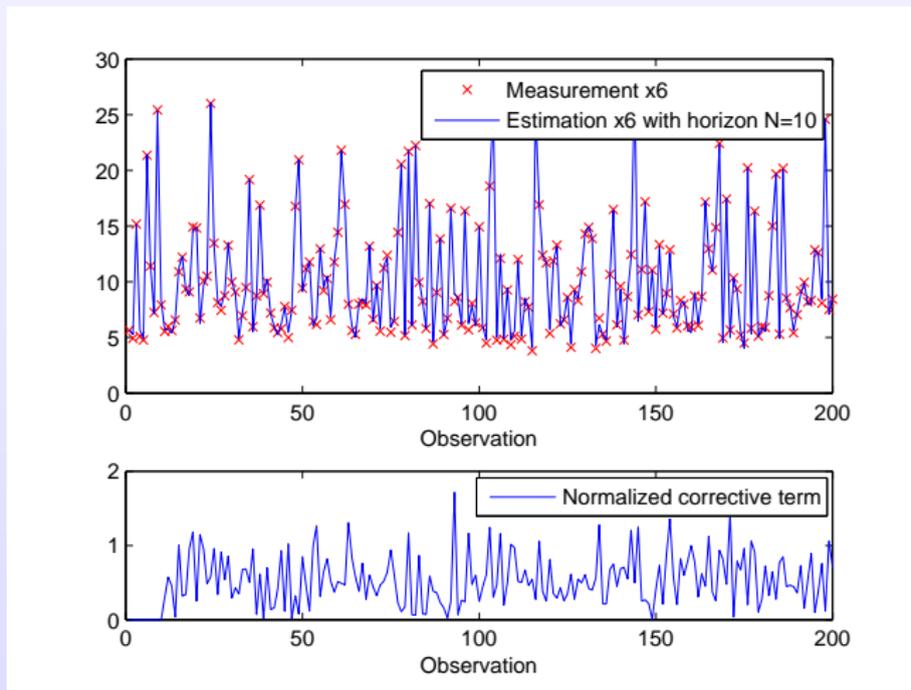


Figure: x_6 state estimation and measurement

3. Application to a simplified BOF process

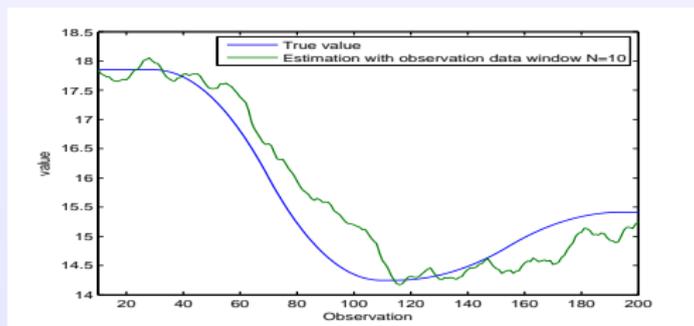


Figure: a_1 parameter estimation

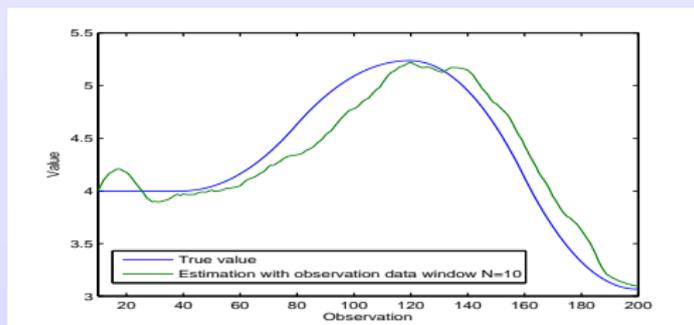


Figure: a_2 parameter estimation

3. Impact of the observation data window length

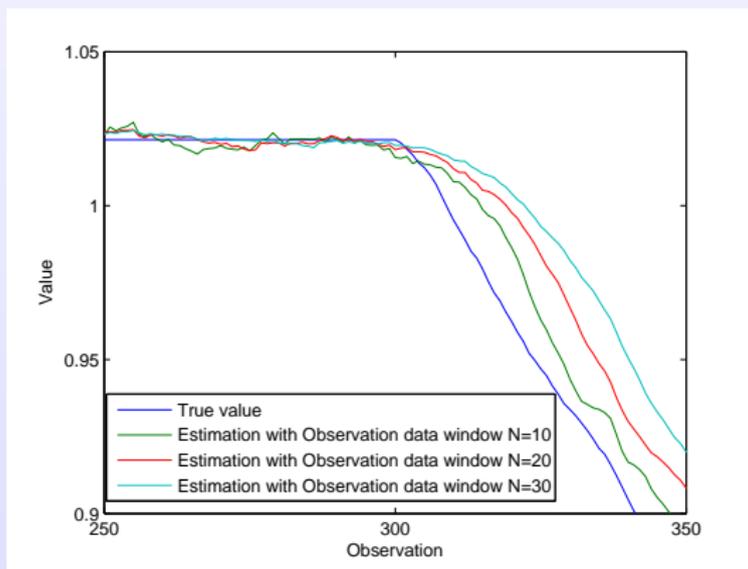


Figure: Impact of the observation data window length on parameter estimation

Compromise between : estimation delay \leftrightarrow measurement noise filtering

4. Data reconciliation may be dangerous !!!

Problem : reconcile raw data is sensitive to outliers
estimated model's parameters may be inapropriated!

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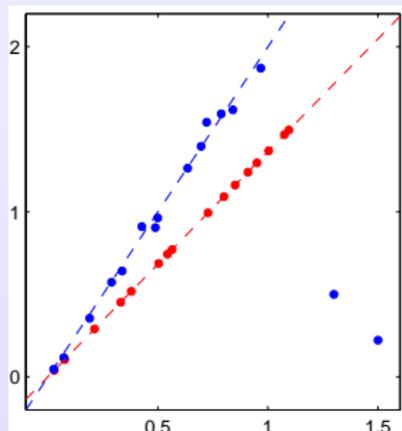


Figure: Outliers influence

Blue color : raw data and theoretical model

Red color : estimated variables and obtained model

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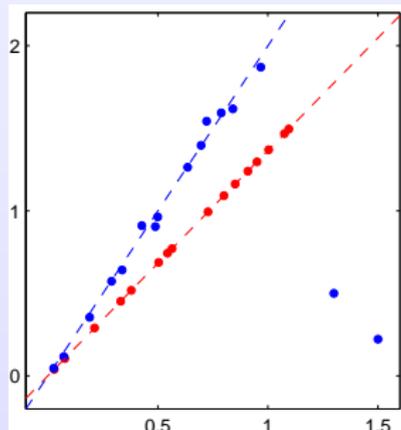


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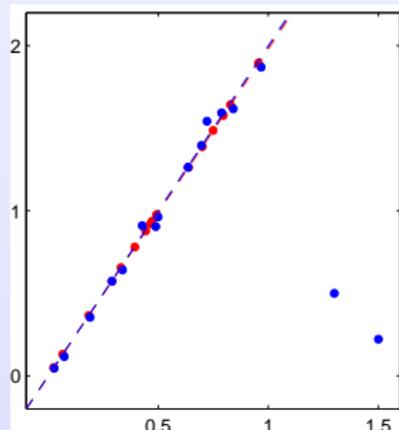


Figure: Removing outliers influence

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Red color : estimated variables and obtained model

4. Gross error rejection

Gross error

- Due to instrument malfunction, miscalibration or drift, leakage/poor sampling
- Precautions: to avoid biased measurement adjustments or estimates

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Method

Let us define the coefficient ratio r_j . Each component $(r_j)_k$ is defined by:

$$(r_j)_k = \frac{(|x_j - \hat{x}_j|)_k}{\sqrt{V(k, k)}}, \quad k = 1, \dots, v$$

If one or several components $(r_j)_k > T$, let us denote $(r_j)_m = \max_k (r_j)_k$
The variance of $(x_j)_m$ is increased to simulate the lack of that measurement for the next sliding windows.

4. Gross error rejection

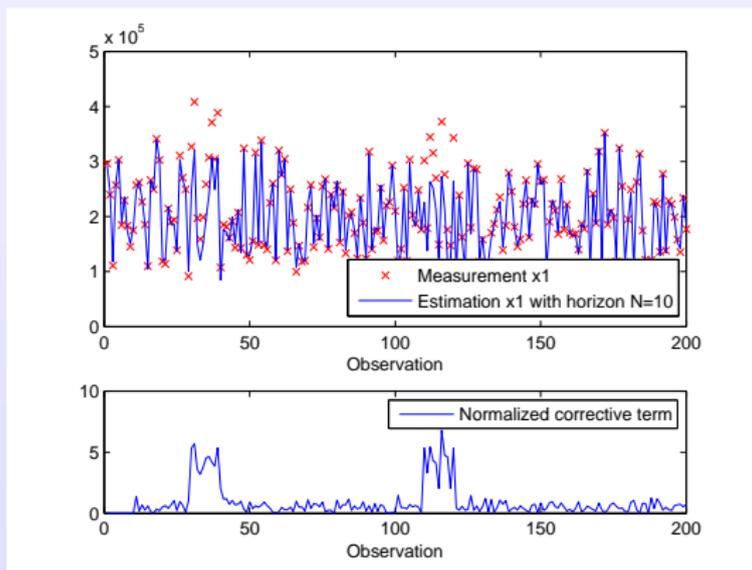


Figure: x_1 state estimation in the presence of a gross error

Conclusion

- Development of a general method for simultaneous data reconciliation and parameter estimation for non-linear models.
- Use of a sliding observation window → to reduce the model parameter estimate sensitivities to measurement errors
- Provide coherent data (state variables + model parameter)
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Perspectives

- Application to a complete BOF model with real data to observe the impact of control set-points adjustment on the next heat
- Using of a bounded error formulation

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Thanks for your attention