

# State estimation for wastewater treatment plant with slow and fast dynamics using multiple models

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## Objectives

1. Propose a state estimation method for two-time scale systems using Multiple Models (MM)
2. Apply it to an activated sludge model reactor

## Interests

1. Ability to use the convexity properties of the MM in order to design observers and control laws for system diagnosis purpose

## Motivation

1. Difficulty to deal with the **modeling complexity** of nonlinear systems
2. Difficulty to model a process under the **singularly perturbed systems**
3. Existence of multiple **time scale dynamics** : identification and separation

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Introduction

## Introduction

Interests to use the Multiple Model  
What is the Multiple Model ?

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

## State estimation method

Identification of slow and fast dynamics  
Singularly perturbed systems  
Unknown input observer

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

## Wastewater treatment

Process and the reduced ASM1 model  
Slow and fast dynamics  
Estimation results

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

## Conclusions and Future prospects

Conclusions

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A. NAGY KISS,  
G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

## Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions

# Introduction

# The interest to use the Multiple Models

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A. NAGY KISS,  
G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics  
Singularly  
perturbed  
systems

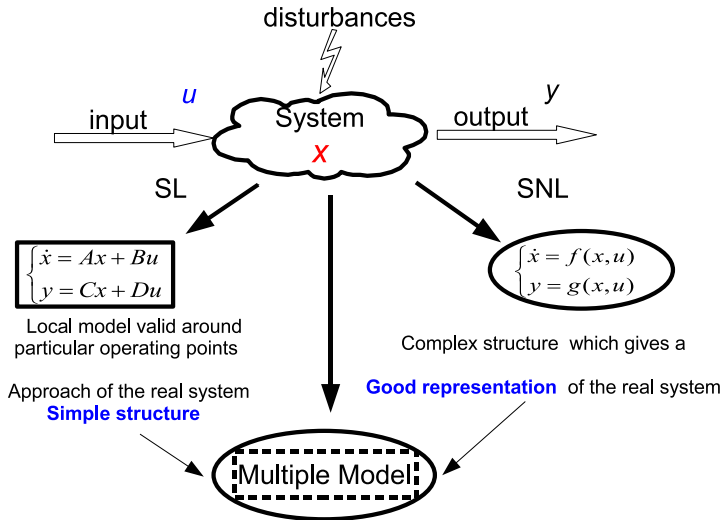
Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions



# What is the Multiple Model ?

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A. NAGY KISS,  
G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems  
Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions

Dynamical system described by a Multiple Model

$$\begin{cases} \dot{x}(t) = \sum_{i=1}^r \mu_i(x(t), u(t)) [A_i x(t) + B_i u(t)] \\ y(t) = \sum_{i=1}^r \mu_i(x(t), u(t)) [C_i x(t) + D_i u(t)] \end{cases}$$

$$\sum_{i=1}^r \mu_i(x, u) = 1 \quad \text{and} \quad \mu_i(x, u) \geq 0$$

**Interest** : this form is particularly attractive for

- stability
- stabilization
- observability studies
- state estimation
- diagnosis

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B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions

# State estimation method

# Identification of slow and fast dynamics

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A. NAGY KISS,  
G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems  
Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

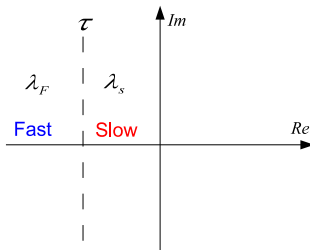
Conclusions

## Homotopy method

Linearization :  $\dot{x}(t) = f(x(t), u(t)) \implies \dot{x}(t) = A_0 x(t) + B_0 u(t)$

$$A_0 = \left. \frac{\partial f(x, u)}{\partial x} \right|_{(x_0, u_0)}, \quad B_0 = \left. \frac{\partial f(x, u)}{\partial u} \right|_{(x_0, u_0)}$$

Order and separate the eigenvalues of  $A_0$  :  $\tau$  - threshold of separation



$$x = \begin{bmatrix} x_F \\ x_S \end{bmatrix}$$



# Singularly perturbed systems

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J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions

## Standard form

$$\epsilon \dot{x}_F(t) = f_F(x_S(t), x_F(t), u(t), \epsilon) \quad (1a)$$

$$\dot{x}_S(t) = f_S(x_S(t), x_F(t), u(t), \epsilon) \quad (1b)$$

where  $\epsilon$  - singular perturbed parameter

**Reduced form :**  $\epsilon \longrightarrow 0$

$$0 = f_F(x_S(t), x_F(t), u(t), 0) \quad (2a)$$

$$\dot{x}_S(t) = f_S(x_S(t), x_F(t), u(t), 0) \quad (2b)$$

## Difficulties :

- ▶ transform a NL system into the singularly perturbed form
- ▶ obtain  $\epsilon$

If possible (for particular cases of SNL), then :

- ▶ resolution of the algebraic system (2a) extract  $x_F$  and replace it in (2b)

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B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions

## Two-time scales

$$\begin{bmatrix} \dot{x}_F(t) \\ \dot{x}_S(t) \end{bmatrix} = \begin{bmatrix} \frac{1}{\epsilon} f_F(x_S(t), x_F(t), u(t), \epsilon) \\ f_S(x_S(t), x_F(t), u(t), \epsilon) \end{bmatrix}$$
$$y(t) = C \begin{bmatrix} x_F(t) \\ x_S(t) \end{bmatrix}$$

equivalent transformation



sector nonlinearity approach

## Multiple model

$$\begin{bmatrix} \dot{x}_F(t) \\ \dot{x}_S(t) \end{bmatrix} = \sum_{i=1}^r \mu_i(x_S, x_F, u) \left\{ \begin{bmatrix} A_{FF}^i & A_{FS}^i \\ A_{SF}^i & A_{SS}^i \end{bmatrix} \cdot \begin{bmatrix} x_F(t) \\ x_S(t) \end{bmatrix} + \begin{bmatrix} B_F^i \\ B_S^i \end{bmatrix} u \right\}$$
$$y(t) = C \begin{bmatrix} x_F(t) \\ x_S(t) \end{bmatrix}$$

# Singularly perturbed systems

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G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions

Consider  $x_F$  as unknown input :  $d(t) = x_F(t)$

$$x(t) = \begin{bmatrix} d(t) \\ x_S(t) \end{bmatrix}$$

Design the matrices :

$$\bar{A}_i = \begin{bmatrix} A_{FF}^i & A_{FS}^i \\ 0 & A_{SS}^i \end{bmatrix} \quad E_i = \begin{bmatrix} 0 \\ A_{SF}^i \end{bmatrix} \quad \bar{C}_S = [0 \quad C_S]$$

$$\begin{cases} \dot{x}(t) = \sum_{i=1}^r \mu_i(\mathbf{x}, u) \cdot [\bar{A}_i x(t) + B_i u(t) + E_i d(t)] \\ y(t) = \bar{C}_S x(t) + C_F d(t) \end{cases} \quad (3)$$

- ▶ Decoupled time scales
- ▶ The estimation of  $x_S$  is made independently of  $x_F$
- ▶ Classic structure of MM affected by unknown inputs
- ▶ **Unmeasurable decision variables**

MM with measurable decision variables :

$$\begin{cases} \dot{x}(t) &= \sum_{i=1}^r \mu_i(\hat{x}, u) \cdot [\bar{A}_i x(t) + B_i u(t) + E_i d(t) + \omega(t)] \\ y(t) &= \bar{C}_S x(t) + C_F d(t) \end{cases}$$

Unknown input observer :

$$\begin{cases} \dot{z}(t) &= \sum_{i=1}^r \mu_i(\hat{x}(t), u(t)) [N_i z(t) + G_i u(t) + L_i y(t)] \\ \hat{x}(t) &= z(t) - H y(t) \end{cases} \quad (4)$$

Dynamic of the state estimation error :  $\dot{e}(t) = \dot{x}(t) - \dot{\hat{x}}(t)$

Under matrix conditions  $\dot{e}(t)$  reduces to :

$$\dot{e}(t) = \sum_{i=1}^r \mu_i(\hat{x}(t)) (N_i e(t) + P \omega(t)) \quad (5)$$

►  $\mathcal{L}_2$  approach

# Unknown input observer

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B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics  
Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions

**Theorem :**  $e(t) \rightarrow 0$  if  $\exists$   $X$ ,  $M_i$  and  $S$  and a positive scalar  $\lambda$  s.t. the following conditions are respected  $\forall i = 1, \dots, r$  :

$$\begin{bmatrix} \bar{A}_i^T (X + S\bar{C}_S)^T + (X + S\bar{C}_S)\bar{A}_i - \bar{C}_S^T M_i^T - M_i \bar{C}_S + I & X + S\bar{C}_S \\ (X + S\bar{C}_S)^T & -\lambda I \end{bmatrix} < 0$$

$$\begin{aligned} SC_F &= 0 \\ (X + S\bar{C}_S)E_i &= M_i C_F \end{aligned}$$

The observer matrices

$$\begin{aligned} H &= X^{-1}S \\ N_i &= (I + H\bar{C}_S)\bar{A}_i - X^{-1}M_i\bar{C}_S \\ L_i &= X^{-1}M_i - N_i H \\ G_i &= (I + H\bar{C}_S)B_i \end{aligned} \tag{6}$$

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G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions

# Wastewater treatment

# Wastewater treatment

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G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

## The diagram of the wastewater treatment plant process

### Introduction

Interests to use the Multiple Model  
What is the Multiple Model ?

### State estimation method

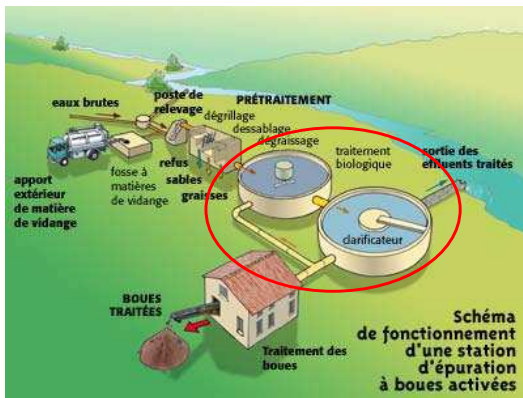
Identification of slow and fast dynamics  
Singularly perturbed systems  
Unknown input observer

### Wastewater treatment

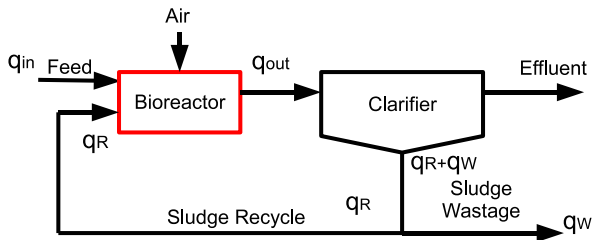
Process and the reduced ASM1 model

Slow and fast dynamics  
Estimation results

### Conclusions



## The diagram of the set biological reactor + clarifier



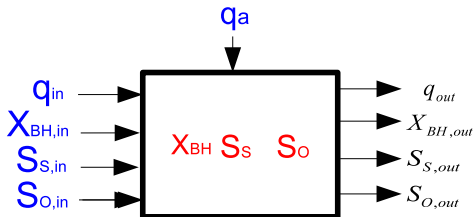
### 1. The operating mode : constant volume

$$q_{out} = q_{in} + q_R$$

### 2. Model : a part of ASM1 $\rightarrow$ carbonated pollution



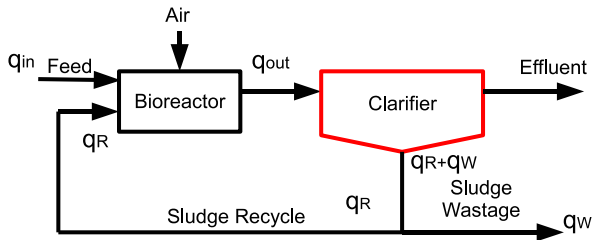
## The reduced ASM1 model : biological reactor



## Simplification hypothesis :

$$\left\{ \begin{array}{l} X_{BH,out}(t) = X_{BH}(t) \\ S_{S,out}(t) = S_S(t) \\ S_{O,out}(t) = S_O(t) \\ S_{O,in}(t) = 0 \end{array} \right.$$

## The diagram of the set biological reactor + clarifier



### 1. Clarifier

$$(q_{in} + q_R)X_{BH} = (q_w + q_R)X_{BH,R}$$

$$S_{S,R} = S_S$$

## The reduced ASM1 model

### Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics  
Estimation  
results

Conclusions

$$\begin{aligned}\dot{S}_S &= \frac{q_{in}}{V} (S_{S,in} - S_S) + (1 - f)b_H X_{BH} - \frac{\mu_H}{Y_H} \frac{S_S}{K_S + S_S} \frac{S_O}{K_{OH} + S_O} X_{BH} \\ \dot{S}_O &= -\frac{q_{in}}{V} S_O + K q_a (S_{O,sat} - S_O) - \frac{1 - Y_H}{Y_H} \mu_H \frac{S_S}{K_S + S_S} \frac{S_O}{K_{OH} + S_O} X_{BH} \\ \dot{X}_{BH} &= \frac{q_{in}}{V} X_{BH,in} - \frac{q_W}{V} \frac{q_{in} + q_R}{q_W + q_R} X_{BH} + \mu_H \frac{S_S}{K_S + S_S} \frac{S_O}{K_{OH} + S_O} X_{BH} - b_H X_{BH}\end{aligned}$$

$$x = \begin{bmatrix} S_S \\ S_O \\ X_{BH} \end{bmatrix} \quad u = \begin{bmatrix} S_{S,in} \\ q_a \\ X_{BH,in} \end{bmatrix}$$

Constants parameters :  $\theta = (\mu_H, b_H, f, Y_H, S_{O,sat}, K_S, K_{OH}, K)$

# Slow and fast dynamics

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G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

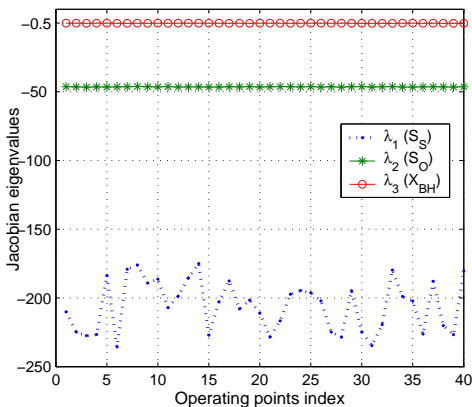
Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions



# State estimation results

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G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

## Introduction

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

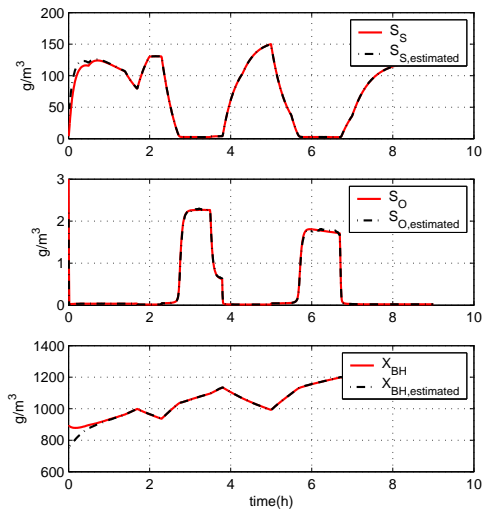
Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions



# Output estimation results

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A. NAGY KISS,  
G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model  
What is the  
Multiple  
Model ?

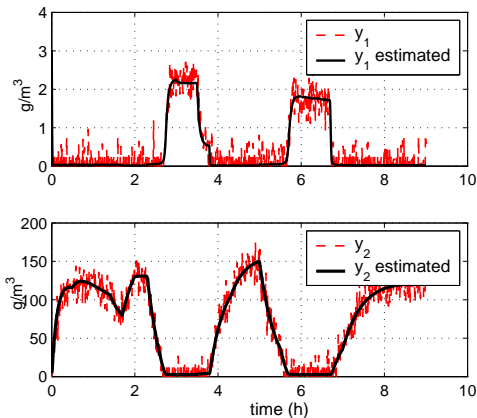
State  
estimation  
method

Identification  
of slow and  
fast dynamics  
Singularly  
perturbed  
systems  
Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model  
Slow and fast  
dynamics  
Estimation  
results

Conclusions



CRAN

A. NAGY KISS,  
G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions

# Conclusions and Future prospects

## Conclusions

1. Identification of slow and fast dynamics
2. Usage of MM with two time scales
3. State estimation using an unknown input observer and MM
4. Application to a part of the ASM1 model of a wastewater treatment plant

## Future prospects

Using the Multiple Model form

1. System Diagnosis :
  - detect
  - isolate faults
  - identify
2. Apply to wastewater treatment plant model



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G. MOUROT,  
B. MARX,  
J. RAGOT,  
G. SCHUTZ

Introduction

Interests to  
use the  
Multiple  
Model

What is the  
Multiple  
Model ?

State  
estimation  
method

Identification  
of slow and  
fast dynamics

Singularly  
perturbed  
systems

Unknown  
input observer

Wastewater  
treatment

Process and  
the reduced  
ASM1 model

Slow and fast  
dynamics

Estimation  
results

Conclusions

**Thank you for your attention**