

State estimation for nonlinear system diagnosis using multiple models. Application to wastewater treatment plants

A. M. Nagy Kiss, B. Marx, G. Mourot, J. Ragot



Nancy-Université

Centre de Recherche en Automatique de Nancy
UMR 7039 CNRS – Nancy-Université
France

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A. M. Nagy
Kiss,
B. Marx,
G. Mourot,
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Objectives

1. Fault diagnosis for complex nonlinear systems
2. Application to the model of an activated sludge bioreactor of a Waste Water Treatment Plant
3. Need for state estimation of environmental plant with limited sensors

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1. Fault diagnosis for complex nonlinear systems
2. Application to the model of an activated sludge bioreactor of a Waste Water Treatment Plant
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Context and tools

1. **modeling complexity** of nonlinear process
 - Multiple Model approach
 - Model uncertainties
2. **corrupted measurement** of the input or output
 - observer based diagnosis
3. **limited number of sensors**
 - unknown input observer design

Outline of the presentation

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Presentation of the wastewater treatment process

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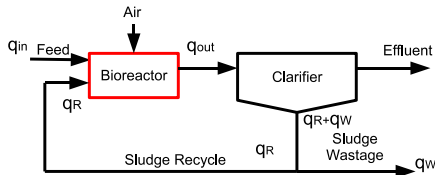
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The **wastewater treatment plant (WWTP)** is composed by :

- a bioreactor
 - ▶ polluted water and bacteria are put in contact and aerated
 - ▶ the bacterial biomass degrades the organic pollution
- a clarifier :
 - ▶ clear water and bacterial biomass are separated
 - ▶ clear water is rejected in the environment
 - ▶ a fraction of the biomass is recycled

The presented study only concerns the bioreactor

- the bioreactor is modelled with the Activated Sludge Model (ASM1)
- the clarifier is supposed to be ideal

Bioreactor description : the Activated Sludge Model (AMS1)

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Nonlinear dynamic system equations :

$$\dot{X}_{DCO}(t) = -\frac{1}{Y_H}(\varphi_1(t) + \varphi_2(t)) + (1 - f_P)(\varphi_4(t) + \varphi_5(t)) + D_1(t)$$

$$\dot{S}_O(t) = \frac{Y_H - 1}{Y_H}\varphi_1(t) + \frac{Y_A - 4.57}{Y_A}\varphi_3(t) + D_2(t)$$

$$\dot{S}_{NH}(t) = -i_{XB}(\varphi_1(t) + \varphi_2(t)) - (i_{XB} + \frac{1}{Y_A})\varphi_3(t) + (i_{XB} - f_P i_{XP})(\varphi_4(t) + \varphi_5(t)) + D_3(t)$$

$$\dot{S}_{NO}(t) = \frac{Y_H - 1}{2.86 Y_H}\varphi_2(t) + \frac{1}{Y_A}\varphi_3(t) + D_4(t)$$

$$\dot{X}_{BH}(t) = \varphi_1(t) + \varphi_2(t) - \varphi_4(t) + D_5(t)$$

$$\dot{X}_{BA}(t) = \varphi_3(t) - \varphi_5(t) + D_6(t)$$

The state variables denote the following concentrations :

$X_{DCO}(t)$: demand in chemical oxygen

$S_O(t)$: dissolved oxygen

$S_{NH}(t)$: dissolved ammonia

$S_{NO}(t)$: dissolved nitrate

$X_{BH}(t)$: heterotrophic biomass

$X_{BA}(t)$: autotrophic biomass

Bioreactor description : the Activated Sludge Model (AMS1)

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with the process kinetics :

$$\varphi_1(t) = \mu_H \frac{X_{DCO}(t)}{K_{DCO} + X_{DCO}(t)} \frac{S_O(t)}{K_{OH} + S_O(t)} X_{BH}(t)$$

$$\varphi_2(t) = \mu_H \eta_{NOg} \frac{X_{DCO}(t)}{K_{DCO} + X_{DCO}(t)} \frac{S_{NO}(t)}{K_{NO} + S_{NO}(t)} \frac{K_{OH}}{K_{OH} + S_O(t)} X_{BH}(t)$$

$$\vdots = \vdots$$

$$\varphi_5(t) = b_A X_{BA}(t)$$

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and the input/output balances :

$$D_1(t) = \frac{q_{in}(t)}{V}(X_{DCO,in}(t) - X_{DCO}(t))$$

$$D_2(t) = -\frac{q_{in}(t)}{V}S_O(t) + K_{qa}(t)(S_{O,sat}(t) - S_O(t))$$

$$\vdots = \vdots$$

$$D_6(t) = -\frac{q_{in}(t)}{V} \frac{f_W(1 + f_R)}{f_W + f_R} X_{BA}(t)$$

Multiple model approach for nonlinear system

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- **Any nonlinear system can be equivalently written as a Multiple Model (MM)** on a compact set of the state space

$$\begin{cases} \dot{x} = f(x, u) \\ y = g(x, u) \\ \text{nonlinear} \end{cases} \Rightarrow \begin{cases} \dot{x} = A(x, u)x + B(x, u)u \\ y = C(x, u)x + D(x, u)u \\ \text{Quasi-LPV} \end{cases} \Rightarrow \begin{cases} \dot{x} = \sum_{i=1}^r \mu_i(x, u)(A_i x + B_i u) \\ y = \sum_{i=1}^r \mu_i(x, u)(C_i x + D_i u) \\ \text{Multiple Model} \end{cases}$$

→ MM with unmeasurable premise variable are generally obtained

1. Nagy, Mourot, Marx, Ragot, Schutz, Systematic multi-modeling methodology applied to an activated sludge reactor model, Industrial & Engineering Chemistry Research, Vol. 46(6), pp. 2790-2799, 2010

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→ MM with unmeasurable premise variable are generally obtained

- ▶ The nonlinearities are rejected in the activating functions $\mu_i(x(t), u(t))$
- ▶ System analysis and design are based on the linear submodels (A_i, B_i, C_i, D_i) with classical tools (Lyapunov functions, LMI, . . .)
- ▶ Different equivalent rewritings may not lead to the same results in terms of controller/observer design¹

1. Nagy, Mourot, Marx, Ragot, Schutz, Systematic multi-modeling methodology applied to an activated sludge reactor model, Industrial & Engineering Chemistry Research, Vol. 46(6), pp. 2790-2799, 2010

Multiple Model of the Activated Sludge Model (AMS1)

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Summing up, the bioreactor is described by a MM with 16 submodels :

$$\begin{aligned}\dot{x}(t) &= \sum_{i=1}^r \mu_i(x, u) [A_i x(t) + B_i u(t)] \\ y(t) &= Cx(t)\end{aligned}$$

- state vector and measured output :

$$\begin{aligned}x^T(t) &= [X_{DCO}(t) \ S_O(t) \ S_{NH}(t) \ S_{NO}(t) \ X_{BH}(t) \ X_{BA}(t)] \\ y^T(t) &= [X_{DCO}(t) \ S_O(t) \ S_{NH}(t) \ S_{NO}(t)]\end{aligned}$$

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$$\begin{aligned}\dot{x}(t) &= \sum_{i=1}^r \mu_i(x, u) [A_i x(t) + B_i u(t) + E_i d(t)] \\ y(t) &= Cx(t) + Gd(t)\end{aligned}$$

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- some incoming pollutants cannot be measured
→ **unknown inputs** $d(t)$:

$$d(t)^T = [S_{NH,in}(t) \ X_{BH,in}(t)]$$

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$$\begin{aligned}\dot{x}(t) &= \sum_{i=1}^r \mu_i(x, u) [(A_i + \Delta A_i(t))x(t) + (B_i + \Delta B_i(t))u(t) + E_i d(t)] \\ y(t) &= Cx(t) + Gd(t)\end{aligned}$$

- ▶ state vector and measured output :

$$\begin{aligned}x^T(t) &= [X_{DCO}(t) \ S_O(t) \ S_{NH}(t) \ S_{NO}(t) \ X_{BH}(t) \ X_{BA}(t)] \\ y^T(t) &= [X_{DCO}(t) \ S_O(t) \ S_{NH}(t) \ S_{NO}(t)]\end{aligned}$$

- ▶ some incoming pollutants cannot be measured
→ **unknown inputs** $d(t)$:

$$d(t)^T = [S_{NH,in}(t) \ X_{BH,in}(t)]$$

- ▶ some model parameters are time varying and not perfectly known
→ **model uncertainties** $\Delta A_i(t)$ and $\Delta B_i(t)$:

$$b_A(t) = b_A + \Delta b_A(t) \text{ and } b_H(t) = b_H + \Delta b_H(t)$$

State and unknown input estimation for uncertain MM

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- The state and unknown input of the uncertain MM :

$$\dot{x}(t) = \sum_{i=1}^r \mu_i(x, u) [(A_i + \Delta A_i(t))x(t) + (B_i + \Delta B_i(t))u(t) + E_i d(t)]$$

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$$y(t) = Cx(t) + Gd(t)$$

- are reconstructed with the following observer :

$$\dot{\hat{x}}(t) = \sum_{i=1}^r \mu_i(\hat{x}, u) \left(A_i \hat{x}(t) + B_i u(t) + E_i \hat{d}(t) + L_i^P (y(t) - \hat{y}(t)) \right)$$

$$\dot{\hat{d}}(t) = \sum_{i=1}^r \mu_i(\hat{x}, u) L_i^I (y(t) - \hat{y}(t))$$

$$\hat{y}(t) = C\hat{x}(t) + G\hat{d}(t)$$

- **Objective :**

find the observer gains : L_i^P and L_i^I minimizing the \mathcal{L}_2 -gain from the inputs $\begin{bmatrix} u(t) \\ d(t) \end{bmatrix}$ to the estimation errors $\begin{bmatrix} e_x(t) \\ e_d(t) \end{bmatrix} = \begin{bmatrix} x(t) - \hat{x}(t) \\ d(t) - \hat{d}(t) \end{bmatrix}$

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$$\hat{y}(t) = C\hat{x}(t) + G\hat{d}(t)$$

- ▶ **Assumptions :**

- constant unknown input : $\dot{d}(t) = 0$
- bounded uncertainties : $\Delta A_i(t) = M_i^a F_a(t) N_i^a$, with $F_a^T(t) F_a(t) \leq I$
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State and unknown input estimation for uncertain MM

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$$\hat{y}(t) = C\hat{x}(t) + G\hat{d}(t)$$

- ▶ **Difficulties :**

the activating functions of the system depend on $x(t)$, while these of the observer depend on $\hat{x}(t)$
the presence of unknown inputs

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- Find a positive definite Lyapunov function $V(e_x, e_d, x)$ such that :

$$\dot{V}(e_x, e_d, x) - \gamma^2 \begin{bmatrix} u(t) \\ d(t) \end{bmatrix}^T \begin{bmatrix} u(t) \\ d(t) \end{bmatrix} + \begin{bmatrix} e_x(t) \\ e_d(t) \end{bmatrix}^T \begin{bmatrix} e_x(t) \\ e_d(t) \end{bmatrix} < 0 \quad (1)$$

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- The proposed quadratic Lyapunov function is :

$$V(e_x, e_d, x) = \begin{bmatrix} e_x(t) \\ e_d(t) \end{bmatrix}^T P_1 \begin{bmatrix} e_x(t) \\ e_d(t) \end{bmatrix} + x^T(t) P_2 x(t)$$

with $P_1 = P_1^T > 0$ and $P_2 = P_2^T > 0$

- Find a positive definite Lyapunov function $V(e_x, e_d, x)$ such that :

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with $P_1 = P_1^T > 0$ and $P_2 = P_2^T > 0$

- LMI optimization allows to find
 - the Lyapunov matrices P_1, P_2
 - the observer gains L_i^P and L_i^I
 - that minimize the \mathcal{L}_2 -gain γ under (1)

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with $P_1 = P_1^T > 0$ and $P_2 = P_2^T > 0$

- LMI optimization allows to find
 - the Lyapunov matrices P_1, P_2
 - the observer gains L_i^P and L_i^I
 - that minimize the \mathcal{L}_2 -gain γ under (1)
- **sufficient LMI conditions are obtained**

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Find matrices $P_1 = P_1^T > 0$, $P_2 = P_2^T > 0$, \bar{P}_j , and scalars $\varepsilon_{1i} > 0$ and ε_{2i} minimizing the scalar $\bar{\gamma} > 0$ under the following LMI constraints

$$\begin{bmatrix} \Phi_{ij}^{11} & \Phi_{ij}^{12} & 0 & \Phi_{ij}^{14} & P_1 \bar{M}_i^a & P_1 \bar{M}_i^b \\ * & \Phi_{ij}^{22} & P_2 B_i & P_2 E_i & P_2 M_i^a & P_2 M_i^b \\ * & * & \Phi_{ij}^{33} & 0 & 0 & 0 \\ * & * & * & -\bar{\gamma} I & 0 & 0 \\ * & * & * & * & -\varepsilon_{1i} I & 0 \\ * & * & * & * & * & -\varepsilon_{2i} I \end{bmatrix} < 0, \quad i, j = 1, \dots, r$$

with

$$\Phi_{ij}^{11} = I + \mathbb{S}(P_1 \bar{A}_j - \bar{P}_j \bar{C}), \quad \Phi_{ij}^{12} = P_1 (\tilde{A}_i - \tilde{A}_j), \quad \Phi_{ij}^{14} = P_1 (\tilde{E}_i - \tilde{E}_j),$$

$$\Phi_{ij}^{22} = \varepsilon_{1i} N_i^{aT} N_i^a + \mathbb{S}(P_2 A_i), \quad \Phi_{ij}^{33} = \varepsilon_{2i} N_i^{bT} N_i^b - \bar{\gamma} I$$

$$\bar{C}^T = \begin{bmatrix} C^T \\ G^T \end{bmatrix}, \quad \bar{A}_i = \begin{bmatrix} A_i & E_i \\ 0 & 0 \end{bmatrix}, \quad \tilde{A}_i = \begin{bmatrix} A_i \\ 0 \end{bmatrix}, \quad \tilde{E}_i = \begin{bmatrix} E_i \\ 0 \end{bmatrix}, \quad \bar{M}_i^a = \begin{bmatrix} M_i^a \\ 0 \end{bmatrix}, \quad \bar{M}_i^b = \begin{bmatrix} M_i^b \\ 0 \end{bmatrix}$$

The observer gains L_j^P and L_j^I , and the \mathcal{L}_2 -gain γ are obtained by :

$$\begin{bmatrix} L_j^P \\ L_j^I \end{bmatrix} = P_1^{-1} \bar{P}_j \quad \gamma = \sqrt{\bar{\gamma}}$$

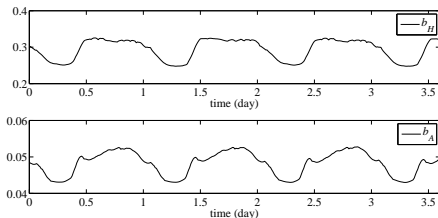
State and unknown input estimation of the ASM1

CRAN

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The proposed observer for MM with unmeasurable premise variables affected by time varying uncertainties and unknown inputs is designed.

The time varying uncertain parameters :



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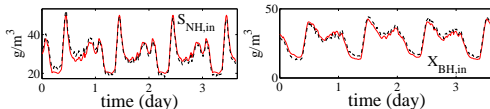
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- The unknown inputs and their **estimates**



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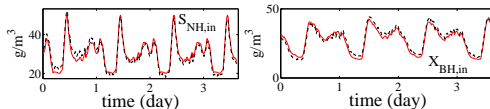
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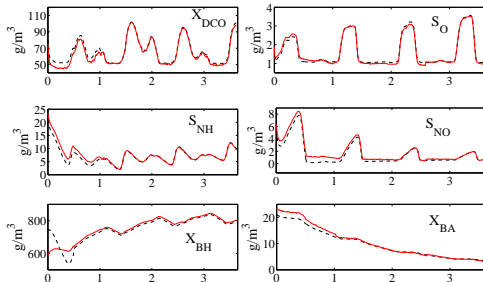
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The proposed observer for MM with unmeasurable premise variables affected by time varying uncertainties and unknown inputs is designed.

► The unknown inputs and their estimates



► The states variables and their estimates



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- ▶ different faults are to be detected and isolated :
 - ▶ output measurement fault (OMF) : $y(t) = Cx(t) + \delta(t)$
 - ▶ input measurement fault (IMF) : $u(t) + \eta(t)$

- ▶ residual generation :
 - by comparing measured and estimated output $r = y - \hat{y}$

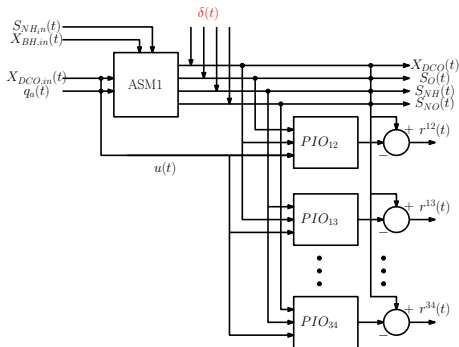
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 - ▶ IMF detection and isolation :
 - each observer is fed with $y(t)$ and a subset subset of $u(t)$
 - the others inputs are considered as unknown inputs
 - the output estimation error is insensitive to the faults affecting the other inputs

Strucured residual generation scheme for OMFDI



The residual signals $r_i^j(t)$ are :

$$r_i^j(t) = y_i(t) - \hat{y}_i^j(t)$$

where j is the observer number and i the component number

Output measurement fault detection and isolation

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- ▶ Residual signals : $r_i^j(t) = y_i(t) - \hat{y}_i^j(t)$
 - ▶ The i^{th} sensor fault, $\delta_i(t)$, ...
 - ▶ affects $y_i(t)$
 - ▶ affects $\hat{y}_k^j(t)$ ($k = 1, \dots, n_y$) if PIO^j is fed with $y_i(t)$
- nothing can be said about r_k^j , when PIO^j is fed with $y_i(t)$

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 - affects $r_i^j(t)$, if PIO^j is not fed with $y_i(t)$
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- ▶ The alarm associated to each fault is :

$$r_{b,i}^j(t) = \begin{cases} 0, & \text{if } |r_i^j(t)| \leq T \\ 1, & \text{if } |r_i^j(t)| > T \end{cases}$$

$$a_i(t) = \prod_{j \in I_i} \left(r_{b,i}^j(t) \prod_{k \neq j, k=1}^{\ell} \bar{r}_{b,k}^j(t) \right)$$

I_i is the index set of observers being not fed with the i^{th} output.

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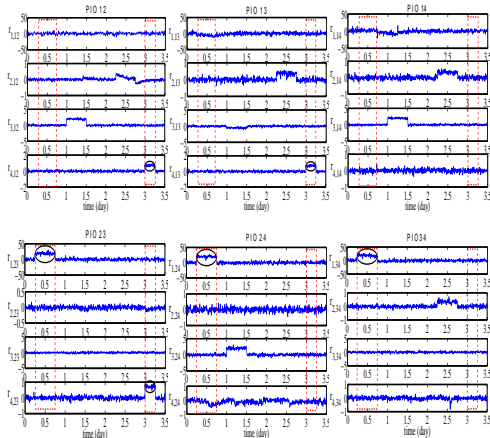
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► sensor faults

- $\delta_1(t)$ affects y_1 , for $t \in [0.25 \ 0.75][\text{days}]$
- $\delta_2(t)$ affects y_2 , for $t \in [2.25 \ 2.75][\text{days}]$
- $\delta_3(t)$ affects y_3 , for $t \in [1 \ 1.5][\text{days}]$
- $\delta_4(t)$ affects y_4 , for $t \in [3 \ 3.25][\text{days}]$



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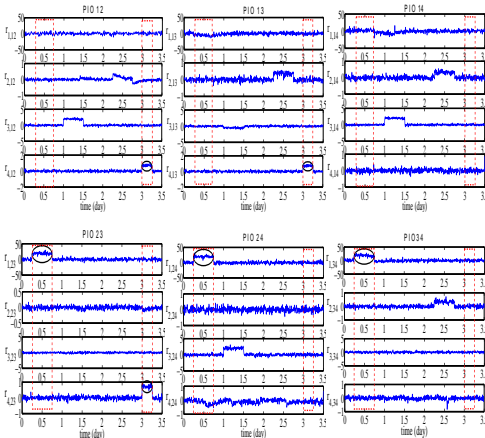
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► sensor faults

► $\delta_1(t)$ affects y_1 , for $t \in [0.25 \ 0.75][\text{days}]$

► PIO^{12} , PIO^{13} and PIO^{14} are fed with y_1

► PIO^{23} , PIO^{24} and PIO^{34} are not fed with y_1

► r_1^{23} , r_1^{24} and r_1^{34} are non null

► r_k^{23} , r_k^{24} and r_k^{34} ($k = 2, \dots, 4$) are null

► $\delta_2(t)$ affects y_2 , for $t \in [2.25 \ 2.75][\text{days}]$

► $\delta_3(t)$ affects y_3 , for $t \in [1 \ 1.5][\text{days}]$

► $\delta_4(t)$ affects y_4 , for $t \in [3 \ 3.25][\text{days}]$

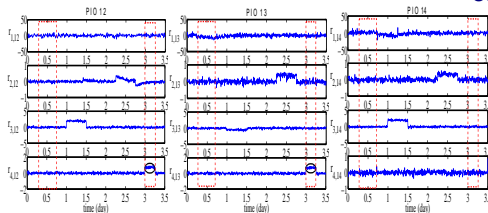
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- ▶ sensor faults

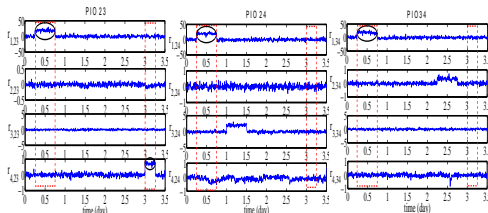


- ▶ $\delta_1(t)$ affects y_1 , for $t \in [0.25 \ 0.75][days]$

- ▶ $\delta_2(t)$ affects y_2 , for $t \in [2.25 \ 2.75][days]$

- $\delta_3(t)$ affects y_3 , for $t \in [1 \ 1.5][days]$

- ▶ $\delta_4(t)$ affects y_4 , for $t \in [3 \ 3.25][days]$



- PIO^{14} , PIO^{24} and PIO^{34} are fed with γ_4

- ▶ PIO^{12} , PIO^{13} and PIO^{23} are not fed with y_4

- r_4^{12} , r_4^{13} and r_4^{23} are non null

- ▶ r_k^{12}, r_k^{13} and r_k^{23} ($k = 1, \dots, 3$) are null

Input measurement fault detection and isolation

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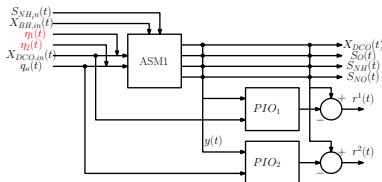
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$$r_i^j(t) = y_i(t) - \hat{y}_i^j(t)$$

where j is the observer number and i the component number

- ▶ each observer is fed with all input except one, considered as unknown input
- ▶ $r_i^j(t)$ ($i = 1, \dots, n_y$) is affected by η_i if PIO^j is fed with u_i
- ▶ $r_i^j(t)$ ($i = 1, \dots, n_y$) is not affected by η_i if PIO^j was designed with u_i as an UI

- ▶ Multiple Model representation of a nonlinear model of a bioreactor
 - ▶ unmeasurable premise variables
 - ▶ model uncertainties
 - ▶ unknown inputs
- ▶ State and unknown input estimation for uncertain MM with UI
 - ▶ proportionnal integral observer
- ▶ Application to fault diagnosis
 - ▶ sensor fault detection and isolation
 - ▶ actuator fault detection and isolation
- ▶ More complex models are under study (with $n = 10$)
- ▶ Estimation error stability conditions should be relaxed

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Thank you for your attention